

認識泵浦性能曲線

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柏努力定律

$$P_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 + \Delta p = P_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2$$

$$P = \rho g h$$

$$\rho g h_1 + \frac{1}{2}\rho v_1^2 + \rho g z_1 + \rho g \Delta H = \rho g h_2 + \frac{1}{2}\rho v_2^2 + \rho g z_2$$

$$\Delta H = (h_2 - h_1) + \frac{1}{2g}(v_2^2 - v_1^2) + (z_2 - z_1)$$

錶壓力差

速度頭差

錶位差

量測結果

項次	流量 (m ³ /h)	轉速 (r/min)	入口錶壓(kPa)	出口錶壓(kPa)	速度頭差(m)	揚程 (m)	電機輸入功率(kW)	軸功 (kW)	流功 (kW)	泵效率 (%)	總效率 (%)
1	27.15	1795.00	4.58	548.45	0.01	56.51	39.37	37.55	4.165	11.09	10.58
2	146.15	1795.00	-15.15	544.52	0.18	58.33	48.53	46.30	23.141	49.98	47.68
3	232.07	1792.00	-17.31	538.38	0.46	58.24	58.24	55.56	36.688	66.03	62.99
4	349.35	1781.20	-20.94	505.82	1.05	55.94	70.04	66.82	53.053	79.40	75.75
5	430.97	1780.40	-24.25	470.42	1.60	53.28	77.62	74.05	62.334	84.18	80.30
6	518.45	1784.20	-28.66	422.66	2.32	49.65	83.92	80.06	69.885	87.29	83.28
7	572.72	1788.00	-31.92	387.32	2.83	46.95	86.82	82.82	72.994	88.13	84.08
8	624.67	1775.21	-35.72	346.64	3.36	43.78	89.70	85.57	74.246	86.77	82.77

1bar=100kpa=10m水柱

10kpa=1m水柱

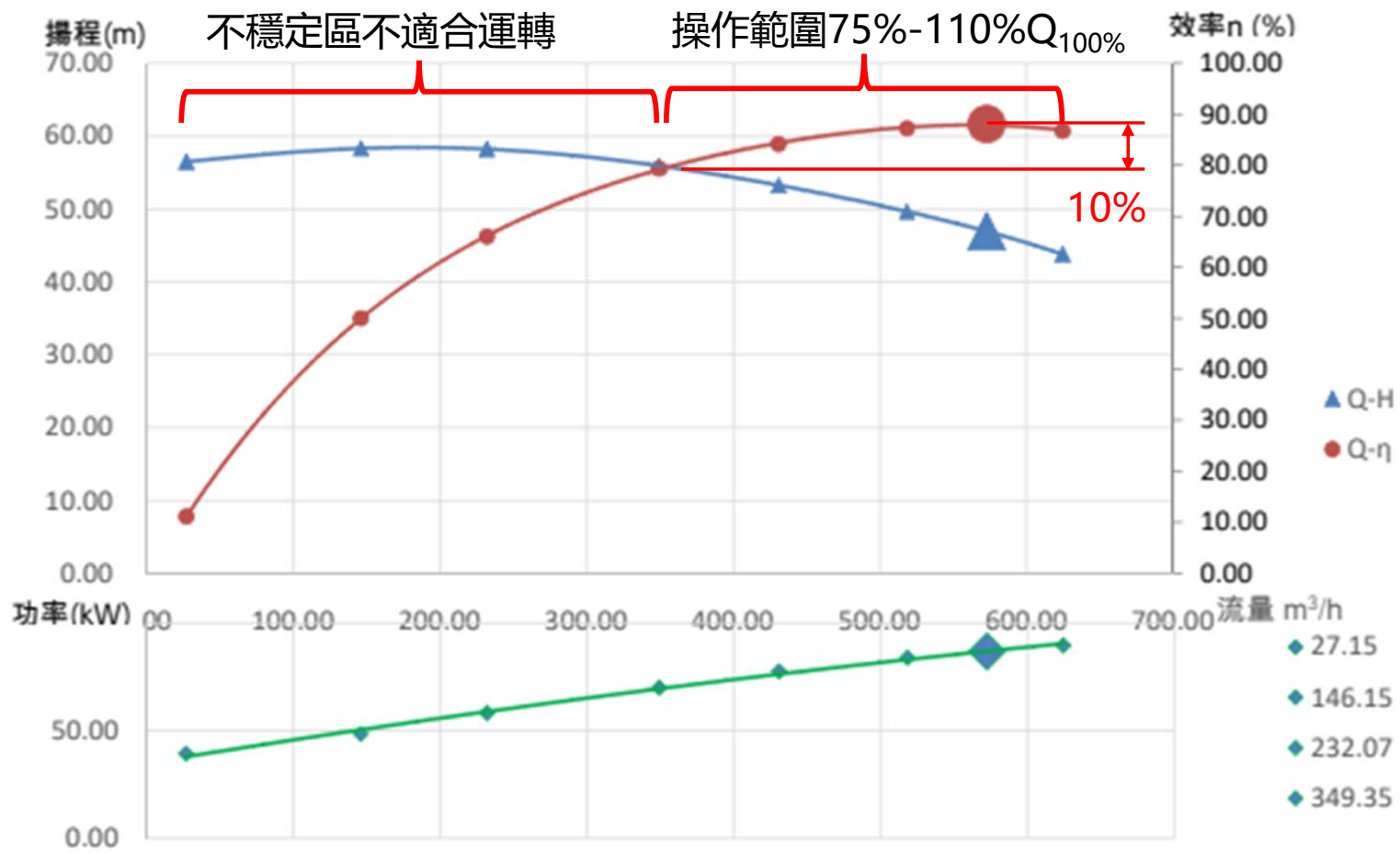
壓差kpa=387.32-(-31.92)=419.24kpa=41.924m 錶位差m=2.2m(未顯示)

速度頭 $m = \frac{V^2}{2g}$ 速度頭差 $m = 4.124 - 1.305 = 2.82$

入口速度頭 $m = \frac{V^2}{2g} = \frac{5.06^2}{2 \times 9.81} = 1.305m$ 出口速度頭 $m = \frac{V^2}{2g} = \frac{8.996^2}{2 \times 9.81} = 4.124m$

揚程 $m = \text{壓差}m + \text{速度頭}m + \text{錶位差}m = 41.924 + 2.82 + 2.2 = 46.944m$

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