Balanced Flow Metering and Conditioning Technology for Fluid Systems (Space Liquid Propulsion Systems) for

2006 Instrumentation Symposium for the Process Industries



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Large Rocket Engine Environments

- Very hot (~6000°F)
- Extreme cold (~ -400°F)
- Vibration
- Volatile fluids (liquid oxygen, etc.)
- High pressures (~7,000 psi.)
- Extreme fluid velocities (flow rates, Reynold's numbers > 10⁷)
- Fast control loops and failure propagation (<3 seconds to full destruction)
- Industry seldom operates in these regimes
- One failed ground test (turbine meter) ~\$200M impact



Problem

- Turbine failure resulted in no LOX flow meter for flight hardware
- Need safe flow metering technology for liquid rocket engines
- Failed past attempts
 - Turbines (work, but severe failure)
 - Vortex shedders
 - Ultrasonic
 - Venturi Tubes (work, but too large for flight)
 - Etc.

NASA Flow Meter Requirements

- Different fluids: LH2, LOX, RP1, etc.
- Different physical states: Gas, Liquid, Multi-Phase
- Wide range (both high and low) in temperature, pressure, vibration and flow conditions
- Very low flow intrusion with near full pressure recovery
- No moving parts
- Minimal piping requirements

- Drop-in replacement of an orifice-plate
- Robust mechanical design
- Highly accurate and repeatable flow measurement
- Easy calibration and maintenance
- Need for high through-put flow areas with low flow restriction

Most needs are common with industrial needs...

Balanced Flow Meter Solution

- NASA patented technology #10/750,628
- Allows engine measurements where none were before
- Ability to condition or measure flow while improving velocity or other profiles
- Provides flow measurement, conditioning, and controlled restriction performance
- Ability to function with minimal straight pipe run
- Measure mass flow rates, fluid volumetric flow rates and density simultaneously
- Sensor set up can provide a triple redundant measurement system
- Successfully fielded by industry

Possible configuration...



- Beta = 0.9
- 7.5" NDP
- Diff. pressure rated at 150 psi

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What is Balanced Flow Technology?

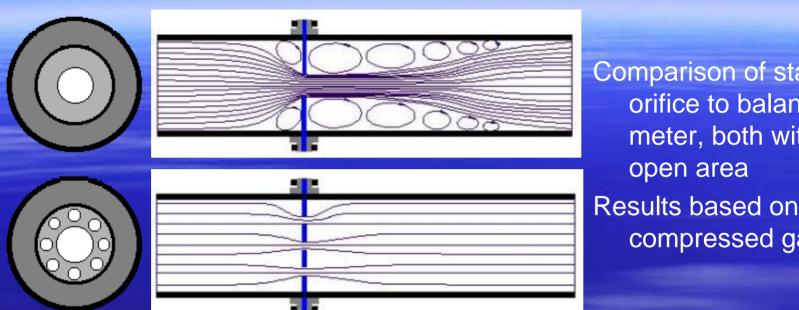
A thin, multi-hole orifice plate with holes sized and placed per a unique set of equations to produce mass flow, volumetric flow, kinetic energy, or momentum BALANCE across the

face of the plate

Chevron-Texaco 18 inch Commercial Plate



How Does It Perform?



Comparison of standard orifice to balanced flow meter, both with 27.1%

compressed gas testing

- 10X better accuracy
- 2X faster pressure recovery (shorter distance)
- 15X noise reduction

- 2.5X less permanent pressure loss
- Exclusively licensed through NASA by A+FlowTek for commercialization

Configurations Tested in 2004



Figure 1 Slotted Configuration



Figure 2 Iron Cross Configuration

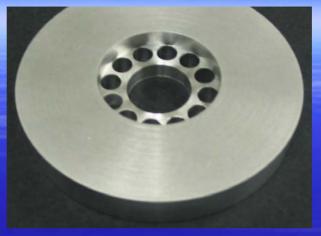


Figure 3 Single Ring of Holes Configuration

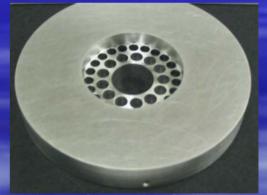


Figure 4 Custom Hole Configuration

Permanent pressure loss, accuracy and discharge coefficient comparable with a Venturi meter!

Balanced Flow Meter Characteristics

- Minimal straight pipe run requirements—BFM has less than 0.5 X pipe diameter straight pipe requirement
- Only requires 0.25 to 0.5 inch thickness and approximately 3 PSI across the plate to condition and monitor flow
- Relatively low cost to build and operate
- Accuracy comparable to Venturi meters
- Cons—similar limitations as standard orifice
 - Not good for pulsing flow
 - Limited turn down
- Testing methods based on American Petroleum Institute (API) Manual of Petroleum Measurement Standards 5.7

How Does it Work?

- Basic design based on multi-hole orifice plate
- Basic relation is the Bernoulli equation
 - Requires custom Cd calculation
 - Long for Bernoulli equation required for high accuracy applications
 - Highest accuracy applications require physical properties models
- Flow proportional to SQRT of delta P Key design factor is the hole distribution

Technical Basis—BFM Hole Layout

Plate hole layout basic equation

$$\kappa \rho A V^n = \text{Constant for each hole} = (\kappa \rho A V^n)_1 = (\kappa \rho A V^n)_2 = ... = (\kappa \rho A V^n)_1$$

At
$$\kappa_1 \rho_1 \sim \kappa_i \rho_{I,}$$

 $A_i/A_1 = (V_1/V_i)^n$

To simplify, let
$$n = 1$$

 $A_i/A_1 = V_1/V_i$

- Example, given a velocity distribution function $V_r/V_{max} = (1 R_r/R_{wall})^{1/7}$
- Radial velocity ratios $V_1/V_1 = ((1 R_1/R_p)/(1 R_i/R_p))^{1/7} = A_i/A_1$

Nomenclature:

- κ: fluid flow correction factor
- ρ: density of fluid
- A: sum of areas at given radius
- V: fluid velocity at radius r
- b: selected balancing constant
- Vmax: velocity at r=0, pipe center
- Rwall: velocity at pipe wall

Technical Basis—BFM Hole Layout Cont.

Subsequent radial areas

$$A_i = A_1((1 - R_1/R_p)/(1 - R_i/R_p))^{1/7}$$

Radial area equation

From
$$\beta^2 = A_{total} / A_{pipe}$$

And multiple holes,
 $A_0 + A_1 + A_2 + \dots + A_n = A_{total} = \beta^2 A_{pipe}$

Hole diameters at radius i

$$D_i = (4A_i/\pi N)^{1/2}$$

Sheer stresses typically lower than standard, single-hole orifice!

Tech Basis-Bernoulli Equation

Bernoulli Equation—longer form $(P_a-P_b)/\rho + g(Z_a-Z_b)/g_c + (\alpha_a V_a^2 - \alpha_b V_b^2)/2g_c - h_{fb} = 0$

Equation of Continuity

$$(\rho AV)_a = m = (\rho AV)_b$$

 Simplified Bernoulli Equation—assume constant density (incompressible), frictionless fluid (zero viscosity), and no elevation changes

$$(P_a-P_b)/\rho + (V_a^2 - V_b^2)/2g_c = 0$$

 Equations from ISO 5167-1, API 14.3.1, etc. Derivations in multiple texts.

Tech Basis-Bernoulli Equation

Beta area ratio

$$(\beta)^2 = A_b/A_a$$

Flow Equation

$$m = C_D Y A_b (2g_c \rho_a (P_a - P_b)/(1 - \beta^4))^{1/2}$$

There can be longer equation forms with many other factors, such as expansion factors, compressibility factors, meter correction factors, etc.

Typical Uncertainties

- Gas Flow: +/- 0.67% (API 14.3.1)
- Liquid Flow: +/- 0.57% (API 14.3.1)
- Spec values are EXTREMELY conservative

BFM Lab Accuracies

- +/- 2% without calibration
- +/- 1.0% long equation
- Calculated +/- 0.1% custom equation, calibrated
- BFM calculated value: +/-0.25% (Directly measured)

MSFC Water Calibration Facility



- National Institute of Standards and Test (NIST) certified
- Volumetric system
- 5000 gallons
- Pump or gravity fed
- Quad deionized water
- 0.25% flow accuracy over unit of time between level sensors
- 0.15% repeatability at given flow set point

MSFC Gas Calibration Facility



- Positive displacement, inverted cylinder system
- NIST certified
- Multiple gases including N, He, Air, Argon, Freon
- 0.01 to 3000 psi operation
- .01 to 400 SCFM
- Accuracy & repeatability???

Cd and K Factor Comparisons

Balanced Flow Meter plate performance,

from minimum flows to sonic

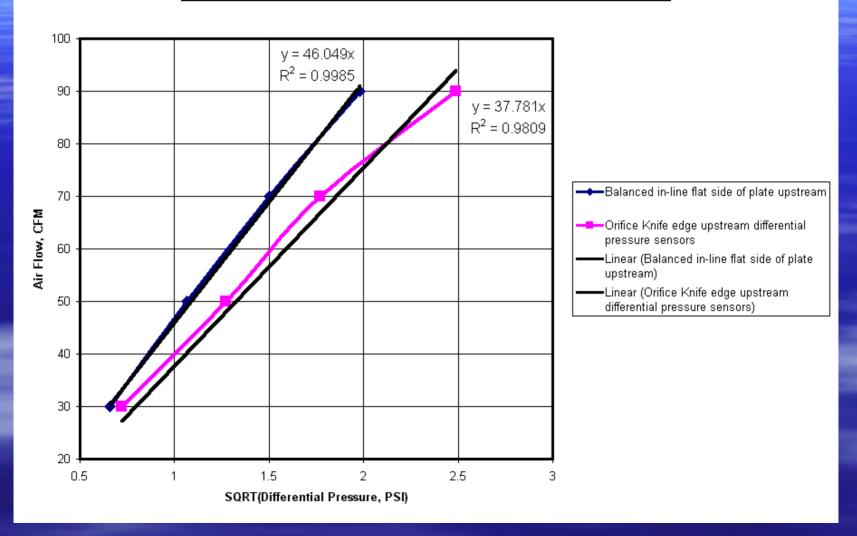
BETA	0.25	0.500	0.521	0.650	0.500 , fouled	0.500,elbow
Avg Cd	0.892	0.882	0.881	0.911	0.824	0.848
Cd Dev	0.032	0.001	0.009	0.010	0.038	0.008
Avg K Val	287.1	16.3	13.2	4.0	15.65	18.63
K Dev	20.8	0.60	0.53	0.16	1.23	0.38

BETA	0.25	0.500	0.521	0.650
Venturi K, Cd=0.96	134.2	5.8	4.7	1.3
Venturi K, Cd=0.80	255.9	12.9	10.7	3.5
BFM K	287.1	16.3	13.2	4.0
Orifice K	669.4	31.5	25.7	7.4

Note: Venturi values do not include downstream losses.

BFM vs. Orifice Flow Equation

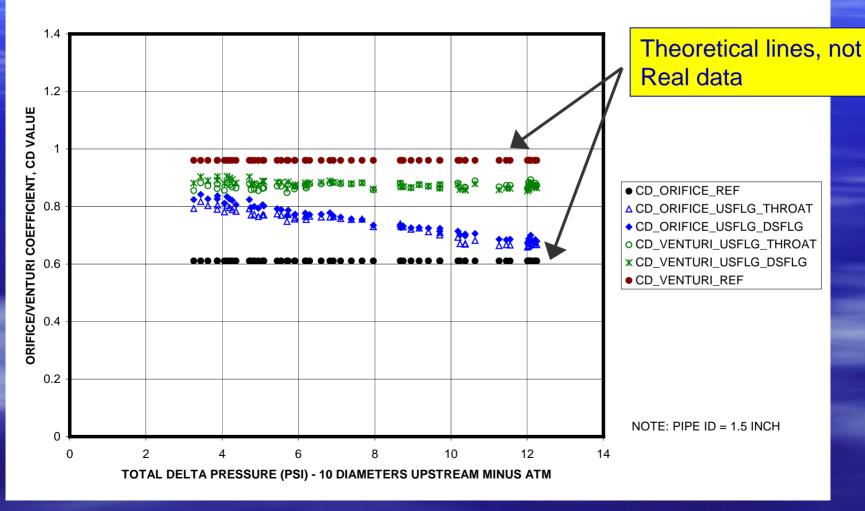
SQRT(Differential Pressure, PSI) versus Air Flow, CFM



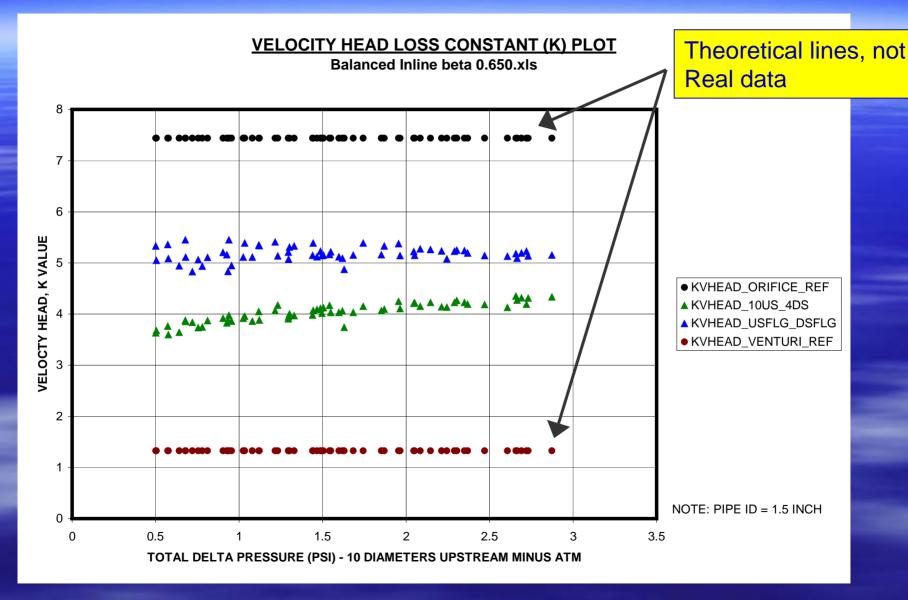
BFM Calibration Cd

ORIFICE/VENTURI COEFFICIENT (Cd) PLOT

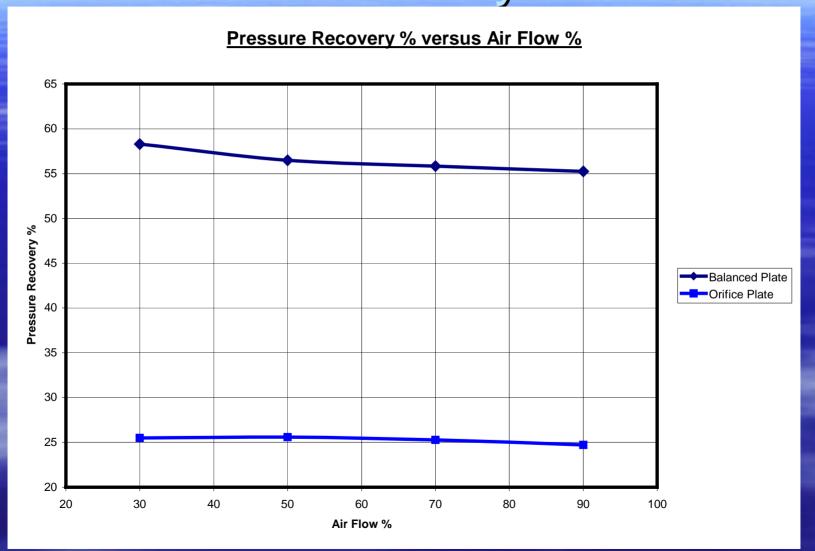
Balanced Inline and Staggered beta 0.500 Flat side upstream.xls



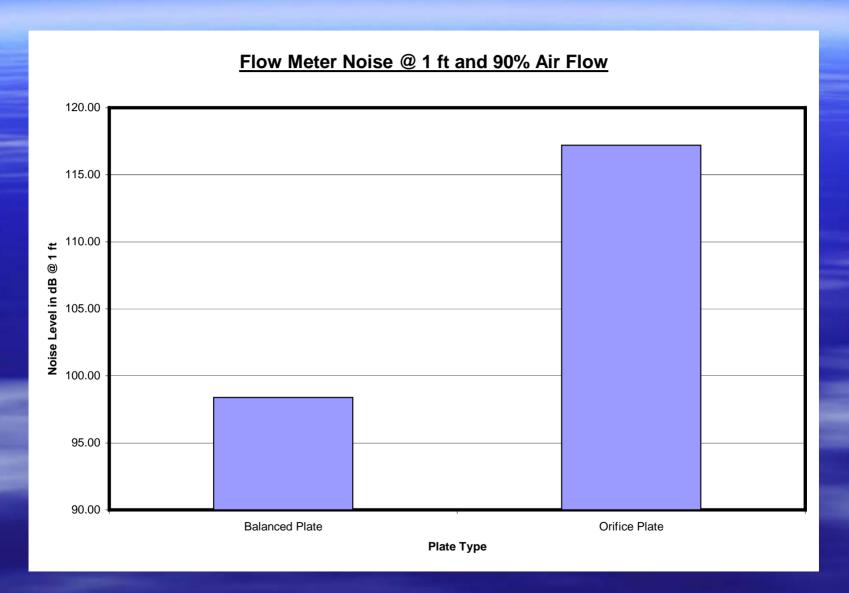
BFM K Factor Plots



BFM vs. Standard Orifice Pressure Recovery



BFM vs. Orifice Acoustic Noise



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Why Does This Matter?

- Believe will meet NASA liquid engine flow meter requirements—test program on-going
- Provides safe, rugged, robust flow meter
- Provides drop-in orifice meter replacement
- Increases fluid system efficiency to save \$\$\$
- Provides multiple benefits with relative low-cost
 - Reduced piping requirements
 - Reduced noise generation (EPA regulations)
 - No moving parts, simple design
 - Capable of simultaneous fluid metering and flow profile conditioning
 - Robust calibration—well defined and characterized traditional techniques
 - Typical +/- 0.15% accuracy of measured flow throughout measurement range
 - Reduced pump energy requirements
 - High pressure recovery
 - Low permanent pressure loss

Lessons Learned

- Always double check flow meter vendor claims, flow equations, and calibration techniques
- There are hundreds of emerging flow metering technologies—stringently define your unique requirements
- Determine best calibration method for your application—in-situ system level calibration vs. typical individual component calibration
- Test/Calibrate as you intend to use the meter—If possible, test your new meter!
- Follow standards for instrument placement, uncertainties, etc., but not for plate thickness!

Useful References

- The Consumer Guide to Differential Pressure Flow Transmitters by David W. Spitzer and Walt Boyes, Published by Copperhill and Pointer, Inc., ISBN 1-932095-03-9
- API Manual of Petroleum Measurement Standards 5.7, Testing Protocol for Differential Pressure Flow Measurement Devices
- API Manual of Petroleum Measurement Standards Ch. 14—Natural Gas Fluids Measurement, Section 3—Concentric, Square-Edged Orifice Meters, Part 1— General Equations and uncertainty Guidelines
- API Manual of Petroleum Measurement Standards Ch. 14—Natural Gas Fluids Measurement, Section 3—Concentric, Square-Edged Orifice Meters, Part 2— Specification and Installation Requirements
- ISO 5167-1 Measurement of fluid flow by means of pressure differential devices inserted in circular cross-section conduits running full, Part 1: General principles and requirements
- ISO 5167-1 Measurement of fluid flow by means of pressure differential devices inserted in circular cross-section conduits running full, Part 2: Orifice Plates
- The measurement, instrumentation, and sensors handbook, John G. Webster, CRC Press & IEEE Press

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